

AMENDMENTS TO THE SPECIFICATIONS

The paragraph at page 3, lines 23-26:

A¹ U.S. Patents 5,128,024 and 5,284,573 issued to R.B. LaPierre et al. and ~~5,294,573~~ issued to N. Haun describe hydrocarbon conversion processes in which heavy oils are simultaneously subjected to hydrocracking and dewaxing using a catalyst based upon zeolite beta with a hydrogenation component.

The paragraph page 10, lines 4-22:

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A The subject hydrocracking process will be operated within the general range of conditions now employed commercially in hydrocracking processes. The operating conditions in many instances are refinery or processing unit specific. That is, they are dictated in large part by the construction and limitations of the existing hydrocracking unit, which normally cannot be changed without significant expense, the composition of the feed and the desired products. The inlet temperature of the of the catalyst bed should be in the range of from about 232 to about 454°C (450-850°F), and the inlet pressure should be above about ~~13500~~ 10,350 kPa (1,500 psig). The feed stream is admixed with sufficient hydrogen to provide hydrogen circulation rate of about 180 to 1335 n./l (1000 to 7500 SCF/Bbl.) and passed into one or more reactors containing fixed beds of the catalyst. The hydrogen will be primarily derived from a recycle gas stream which may pass through purification facilities for the removal of acid gases although this is not necessary. The hydrogen rich gas admixed with the feed and any recycle hydrocarbons will preferably contain at least 90 mol percent hydrogen. For distillate hydrocracking the feed rate in terms of liquid hourly space velocity (L.H.S.V.) will normally be within the broad range of about 0.3 to 1.5 hr⁻¹, with a L.H.S.V. below 1.2 being preferred.